

SPECIFICATION

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[SYSTEM FOR IN-SITU GENERATION OF FLUORINE RADICALS AND/OR FLUORINE- CONTAINING INTERHALOGEN (XF_n) COMPOUNDS FOR USE IN CLEANING SEMICONDUCTOR PROCESSING CHAMBERS]

Background of Invention

[0001] *BACKGROUND OF THE INVENTION* OLE_LINK2 OLE_LINK1 *Field of the Invention* The invention relates to a system and method for *in-situ* generation of fluorine radicals and/or fluorine-containing interhalogen compounds for use in semiconductor manufacturing processes, such as removal of solid residues or particles from semiconductor equipment.

[0002] OLE_LINK2OLE_LINK1 *Description of the Related Art* Semiconductor processing generally involves decomposition of relatively volatile precursors containing silicon (Si), tungsten (W), titanium (Ti), or tantalum (Ta) to form complex metal oxides or silicates. Such volatile precursors are notorious for forming solid residues inside the semiconductor processing chamber or on other internal components of the chamber, such as wafer carders, wafer transport mechanisms, and wafer platens.

[0003] As such, solid residues accumulate on the internal surfaces of the processing chamber, and solids occasionally flake off from the solid residue deposits to yield free particles floating inside the processing chamber. These free particles, when landing

on semiconductor wafers, result in wafer contamination.

- [0004] It therefore is desirable to remove accumulated solid residues from the interior wall surfaces and other internal parts of the processing chamber, without attacking the structural components of the processing chamber.
- [0005] Convention methods used for cleaning semiconductor processing chambers and reactors include wet scrubbing and plasma-enhanced cleaning.
- [0006] Wet scrubbing methods require disassembling each component part of the processing equipment, scrubbing each part with harsh chemical reagent(s) such as HF, H_2SO_4 , H_3PO_4 , and HNO_3 , rinsing the component parts with large volumes of deionized water, and reassembling those component parts.
- [0007] Such approach has many inherent problems, including: the labor and time required for disassembling, cleaning, and reassembly; the high Mean-Time Off Line (MTOL) as a concomitant of the duration of the cleaning operation; the high volume of hazardous chemicals used; the risk of residual contamination; the incidence of excessive surface wear during the cleaning process; and the potential health issues related to worker exposure to hazardous chemicals.
- [0008] Another conventional method for cleaning semiconductor processing chambers involves use of plasmas formed by applying radio frequency (RF) energy to perfluorinated precursors, such as CF_4 , NF_3 , C_2F_6 , C_2F_8 , and SF_6 . The plasmas thus formed will react with the accumulated solid residues inside the semiconductor processing chamber.
- [0009] Perfluorinated (PFC) gases, however, are among the six strongest greenhouse gases targeted by the Kyoto Climate Protection Protocol of 1997. They generally have global warming potentials (GWPs) three (3) and four (4) orders of magnitude higher than CO_2 . Further, they are extremely stable molecules, tending to stay unchanged in the atmosphere for thousands of years. Moreover, most chamber cleaning systems utilizing plasma-enhanced cleaning techniques have low gas decomposition rates, resulting in high levels of PFC gases being released into the atmosphere.
- [0010] Plasmaless or dry cleaning processes using chlorine trifluoride (ClF_3) and other

fluorine radicals and/or fluorine-containing interhalogens have recently proved to be effective in removing solid residues from semiconductor processing chamber. ClF_3 and other fluorine radicals and/or fluorine-containing interhalogens react with such solid residues to form volatile reaction products, which can be readily removed from the processing chamber by vacuum or other devices. See Y. Saito et al., "Plasmaless Cleaning Process of Silicon Surface Using Chlorine Trifluoride", Applied Physics Letters, vol. 56(8), pp. 1119-1121 (1990); *also see* D.E. Ibbotson et al., "Plasmaless Dry Etching of Silicon with Fluorine-Containing Compounds", Journal of Applied Physics, vol. 56(10), pp. 2939-2942 (1984); *also see* Ashley U.S. Patent No. 5,565,038 entitled "Interhalogen Cleaning of Process Equipment," issued October 15, 1996.

- [0011] The use of fluorine radicals or fluorine-containing interhalogens for cleaning of semiconductor processing equipment, however, faces practical problems of implementation and commercial viability.
- [0012] For example, the supply of fluorine radicals or fluorine-containing interhalogens, including ClF_3 , are highly corrosive, and issues such as compatibility of storage and dispensing vessels, and associated process piping and componentry, require substantial attention and costly solutions.
- [0013] Further, interhalogen compounds are extremely irritating to human respiratory tracts. The threshold level of human tolerance of ClF_3 vapor is as low as 100 ppb, and an LC 50, 1 hour of 300 ppm. Inadvertent leakage of such highly toxic fluid is therefore highly hazardous to human health. Further, most interhalogen compounds are liquids at room temperature and are transported in the liquid phase, and the inherent high density of liquids over gases accentuates many of the risks associated with transporting such compounds.
- [0014] Thus, it would be a significant advance in the art to provide a system and method that generates fluorine radicals and/or fluorine-containing interhalogens with minimized risk of exposure to these compounds and that overcomes problems otherwise associated with transporting and storing highly reactive fluorine radicals and fluorine-containing interhalogens.

Summary of Invention

- [0015] *SUMMARY OF THE INVENTION* The present invention broadly relates to a system and method for *in-situ* generation of fluorine radicals (hereinafter "F radicals") and/or fluorine-containing interhalogen compounds (hereinafter " XF_n ", wherein X is Cl, Br, or I, and $n = 1, 3, 5$, or 7) using materials that are less hazardous than ClF_3 .
- [0016] A specific aspect of the present invention relates to an *in-situ* fluorine radicals and/or fluorine-containing interhalogen compounds (e.g., XF_n compounds) generation system for use in semiconductor manufacturing processes, such system comprising:
- [0017] (a) a fluorine source for supplying fluorine gas;
- [0018] (b) a halogen source for supplying at least one halogen species selected from the group consisting of Cl_2 , Br_2 , and I_2 ;
- [0019] (c) a processing chamber communicatively connected with the fluorine source and the halogen source; and
- [0020] (d) an energy source for supplying external energy to facilitate generation of fluorine radicals and/or fluorine-containing interhalogen compounds.
- [0021] The energy source in such system can be of any suitable type, providing the appropriate energy for the process. For example, the energy generated by the energy source can comprise photoenergy or thermal energy. Ultraviolet (hereinafter UV) light having a wavelength from about 100 nm to about 400 nm is one type of photoenergy that is particularly effective in enhancing the reaction rate of fluorine gas and other halogen species to yield F radicals and/or XF_n by photolysis.
- [0022] Any suitable type of UV light generators well known in the art can be used for practicing the present invention, as is readily determinable by a person ordinarily skilled in the art without undue experimentation. For example, such UV generators may comprise hydrogen lamps, deuterium lamps, xenon discharge lamps, electric arcs, discharge tubes, incandescent devices, flash tubes, pulsed lasers, and the like.
- [0023] In a specific embodiment of the present invention, the fluorine gas and the halogen species are separately transported into the processing chamber and mixed therein to form F radicals and/or XF_n . In such manner, the processing chamber to be

cleaned subsequently functions as reaction chamber for the fluorine gas and the halogen species. F radicals and/or XF_n species locally formed in such processing chamber subsequently react with solid residues accumulated in such processing chamber and effect removal of those solid residues.

[0024] Therefore, the external energy source is communicatively connected to the processing chamber to supply external energy to the processing chamber, to effectively facilitate reaction of fluorine and other halogen species. In order to efficiently control the reaction process, the processing chamber comprises temperature/pressure monitoring and controlling devices. The reaction temperature inside the processing chamber is generally controlled within the range from about room temperature (i.e., about 20 ° C) to about 350 ° C, preferably from about room temperature to about 100 ° C when photoenergy is primarily supplied, or from about 280 ° C to about 350 ° C when thermal energy is primarily supplied. Pressure in the processing chamber is controlled within a range from about 1 Torr to about 1000 Torr.

[0025] In an alternative embodiment of the present invention, the fluorine gas and the halogen species are mixed before entering the processing chamber, either in fluid delivery conduits or in a separate mixing chamber.

[0026] Preferably, the *in-situ* generation system of the present invention further comprises a separate mixing chamber upstream the processing chamber. Fluorine gas and other halogen species are first flowed into such mixing chamber to form F radicals and/or XF_n compounds. The formed F radicals and/or XF_n compounds are subsequently transported into the processing chamber to react with accumulated residues in the processing chamber for the purpose of removing such residues.

[0027] When such separate mixing chamber is employed, the energy source will supply photoenergy or thermal energy directly to such mixing chamber. Similarly, such mixing chamber may comprise temperature/pressure monitoring and controlling devices for effective control of reaction conditions as specified hereinabove.

[0028] In a more preferred embodiment, the *in-situ* generation system comprises a separate holding chamber between said mixing chamber and said processing

chamber. The F radicals and/or XF_n gases formed in the mixing chamber may be flowed first into the holding chamber and stored therein until a pre-determined pressure threshold is reached. Such holding chamber serves to allow immediate gas flow to the processing chamber on demand and to shorten the "waiting-period" associated with generation startup or reaction initialization. The holding chamber may further comprise flow-regulating devices, such as a mass flow controller, to achieve reproducible delivery of F radicals and/or XF_n compounds into the processing chamber.

[0029] Furthermore, such *in-situ* generation system may comprise an exhaust/abatement system downstream of said processing chamber to receive an effluent gas stream discharged by the processing chamber.

[0030] In another preferred embodiment of the present invention, the *in-situ* generation system comprises at least one bypassing line for flowing the fluorine gas and halogen species, either separately or in mixture, without passing through the processing chamber. Such bypassing line enables stable fluid flow within the system, regardless of whether the processing chamber is in a cleaning stage or a wafer-processing stage (during which time the processing chamber is isolated from the *in-situ* generation system). More preferably, such bypassing line functions to circulate unmixed fluorine gas and halogen species back to the fluorine and halogen source vessels for recycling.

[0031] In yet another preferred embodiment of the present invention, the *in-situ* generation system comprises a diluent gas source connected with the processing chamber for supplying a relatively inert gas to dilute the generated F radicals and/or XF_n compounds. Because F radicals and/or interhalogen compounds react with solid residues in the processing chamber at an exceedingly rapid rate, forming gaseous end products, the use of pure F radicals and/or interhalogen fluids generated can cause over-pressurizing of the processing chamber. Such over-pressurizing can in turn lead to fluctuation of internal pressure or, more seriously, rupture of the process chamber, or leakage therefrom. Therefore, it is desirable to employ a relatively inert gas to dilute the F radicals and/or XF_n compounds to reduce the reaction rate.

[0032] The term "relatively inert gas" as used herein refers to gases that are non-reactive or that react only insignificantly with the solid residues inside the processing

chamber. Such gases include, but are not limited to, Ar, He, and N_2 . N_2 is a preferred diluent for the practice of the present invention.

[0033] A specific aspect of the present invention relates to an apparatus for generating ClF_3 , comprising:

[0034] (a) a fluorine gas source;

[0035] (b) a chlorine gas source;

[0036] (c) a mixing chamber communicatively connected with said fluorine gas source and the chlorine gas source, for mixing fluorine and chlorine gases;

[0037] (d) a photoenergy source for supplying photoenergy to said mixing chamber to facilitate generation of chlorine trifluoride therein; and

[0038] (e) a processing chamber connected with said mixing chamber.

[0039] Another specific aspect of the present invention relates to an apparatus for generating ClF_3 , comprising:

[0040] (a) a fluorine gas source;

[0041] (b) a chlorine gas source;

[0042] (c) a processing chamber communicatively connected with said fluorine gas source and the chlorine gas source; and

[0043] (d) a photoenergy source for supplying photoenergy to the processing chamber to facilitate generation of chlorine trifluoride therein.

[0044] Yet another aspect of the present invention relates to a method for *in-situ* generation of F radicals and/or XF_n compounds for use in a semiconductor manufacturing process, comprising the steps of:

[0045] (a) providing a fluorine source for supplying fluorine gas;

[0046] (b) providing a halogen source for at least one halogen species selected from the group consisting of Cl_2 , Br_2 , and I_2 ;

[0047] (c)flowing the fluorine gas and the halogen species into a processing chamber communicatively connected with the fluorine source and the halogen source; and

[0048] (d)generating fluorine radicals and/or fluorine-containing interhalogen compounds by supplying external energy to the fluorine gas and/or the halogen species.

[0049] A further aspect of the present invention relates to a method of generating ClF_3 , for cleaning of a processing chamber, comprising the steps of:

[0050] (a)providing a fluorine gas source;

[0051] (b)providing a chlorine gas source;

[0052] (c)mixing fluorine and chlorine gases in a mixing chamber communicatively connected with said fluorine gas source and said chlorine gas source;

[0053] (d)supplying photoenergy to said mixing chamber from a photoenergy source to generate chlorine trifluoride in such mixing chamber; and

[0054] (e)flowing chlorine trifluoride from the mixing chamber into the processing chamber.

[0055] A still further aspect of the present invention relates to a method of generating ClF_3 , comprising the steps of:

[0056] (a)providing a fluorine gas source;

[0057] (b)providing a chlorine gas source;

[0058] (c)flowing fluorine gas and chlorine gas from said gas sources into a processing chamber; and

[0059] (d)supplying photoenergy to said processing chamber from a photoenergy source to generate chlorine trifluoride in such processing chamber.

[0060] Another aspect of the present invention relates to a system for generating fluorine radicals and/or fluorine-containing interhalogen compounds, comprising a fluorine source, a halogen source for supplying at least one halogen species other than

fluorine, an enclosure for mixing fluorine with said halogen species other than fluorine, and a photoenergy source for supplying photoenergy to said enclosure. The fluorine-containing interhalogen compounds have a general formula XF_n , wherein X = Cl, Br, or I, and n = 1, 3, 5, or 7. The photoenergy supplied by said photoenergy source may comprise ultraviolet light having a wavelength from about 100 nm to about 400 nm and intensity in a range of from about 10^3 W/m^2 to about 10^6 W/m^2 .

[0061] In a yet further aspect, the present invention relates to a method for generating fluorine radicals and/or fluorine-containing interhalogen compounds, comprising the steps of providing a fluorine source and a halogen source for supplying fluorine and at least one halogen species other than fluorine, mixing fluorine with the halogen species in an enclosure, and supplying photoenergy to the enclosure from a photoenergy source to generate fluorine radicals and/or fluorine-containing interhalogen compounds. The fluorine-containing interhalogen compounds have a general formula XF_n , wherein X = Cl, Br, or I, and n = 1, 3, 5, or 7. The photoenergy supplied by the photoenergy source preferably comprises ultraviolet light.

[0062] Other aspects, features, and embodiments of the invention will be more fully apparent from the ensuing disclosure and appended claims.

[0063]

Brief Description of Drawings

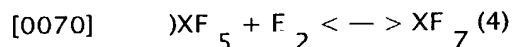
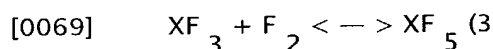
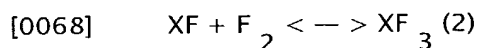
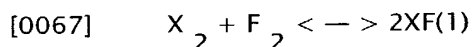
[0064] *BRIEF DESCRIPTION OF THE DRAWINGS* Figure 1 is a diagrammatic illustration of *in-situ* F radical and/or XF_n generation system according to one embodiment of the invention.

[0065] Figure 2 is a diagrammatic illustration of another specific embodiment of an *in-situ* F radical and/or XF_n generation system.

Detailed Description

[0066] *OLE_LINK3DETAILED DESCRIPTION OF THE INVENTION, AND PREFERRED EMBODIMENTS THEREOF* F-containing interhalogens, including ClF_3 , are molecular compounds of fluorine with other halogens. They can be formed by reacting fluorine

gas with another halogen species, according to the following equations:



[0071] (X = Cl, Br, or I)

[0072] The present invention provides an *in-situ* generation system for locally and on-demand generation of fluorine-containing interhalogens through direct combination of fluorine gas with other halogen elements, under controlled reaction conditions. Such local and on-demand generation of interhalogens overcomes many hazards associated with transporting, facilitating, and storing highly reactive fluorine-containing interhalogens.

[0073]

[0074] The *in-situ* generation system of the present invention comprises a fluorine source and a halogen source for supplying at least one halogen species other than fluorine. The fluorine and halogen sources may be *in-situ* generators of fluorine and halogens. Use of such *in-situ* generators further reduces risks associated with transporting and storage of the reactive fluorine and other halogen species.

[0075] The fluorine gas and other halogen species supplied can be mixed either in the semiconductor processing chamber or immediately before entering the processing chamber to form F radicals or XF_n compounds for cleaning such processing chamber.

[0076] Although fluorine gas is capable of reacting with other halogen species at room temperature, the major reaction product formed at such temperature is XF, according to equation (1), and the reaction rate is relatively slow.

[0077] In order to fasten the reaction or to obtain a reaction product characterized by higher fluorine ratio as in equations (2), (3), and (4), external energy is utilized to achieve a favorable reaction equilibrium.

[0078] Accordingly, the *in-situ* system of the present invention advantageously comprises an energy source for supplying external energy to facilitate formation of XF_n compounds at a higher reaction rate and a higher fluorine incorporation rate.

[0079] The energy source may supply thermal energy to the mixture of fluorine gas and other halogen species to enhance reaction rate and fluorine incorporation rate. If thermal energy is the primary energy supplied, it is desirable to maintain the reaction temperature within a range of from about 280 ° C to about 350 ° C and the reaction pressure within a range of from about 1 Torr to about 1000 Torr. Useful thermal energy sources include, but are not limited to, electric heaters, heater exchangers, and radiators.

[0080] It has been found that photoenergy can be supplied in place of thermal energy to enhance reaction kinetics. Specifically, ultraviolet-irradiation has been discovered to significantly enhance the reaction rate between fluorine gas and other halogen species as well as to achieve production yields of XF_n compounds with $n > 1$, in the absence of any external heating.

[0081] Photoenergy is substantially more efficient and is used to achieve a higher energy input to the irradiated atoms and molecules, compared with use of thermal energy. Further, thermal energy dissipates much faster than photoenergy and therefore has a higher waste rate. Finally, use of photoenergy reduces risks associated with pressure-fluctuation caused by thermal heating of an enclosure filled with gases.

[0082] Accordingly, the *in-situ* generation of the present invention preferably uses photoenergy supplied by a photoenergy source.

[0083] More preferably, such photoenergy comprises ultraviolet light having a wavelength in a range of from about 100 nm to about 400 nm and an energy density of from about 10^3 W/m^2 to about 10^6 W/m^2 .

[0084] Any suitable type of UV light generators well known in the art may be used for practicing the present invention, including but not limited to hydrogen lamps, deuterium lamps, xenon discharge lamps, electric arcs, discharge tubes, incandescent devices, flash tubes, pulsed lasers, and the like.

- [0085] When photoenergy is the primary energy supplied, the reaction temperature of fluorine gas and other halogen species may be maintained within a lower range of from about room temperature (i.e., about 20 ° C) to about 100 ° C.
- [0086] Additional heating may be utilized concurrently with the photoenergy, but it is not required. The reaction will readily proceed with satisfactory speed and production yield without such external heating.
- [0087] Mixing and reacting of precursor gases may be accomplished directly within the processing chamber, or immediately before entering into the processing chamber.
- [0088] In one specific embodiment of the present invention, the precursor gases are flowed separately into the processing chamber and mixed therein to form F radicals and/or XF_n compounds. In such embodiment, formation of F radicals and/or XF_n is carried out concurrently with cleaning of the processing chamber. The energy source directly supplies external energy to the processing chamber to facilitate reaction of precursor gases.
- [0089] Supplying external energy directly to the processing chamber provides several advantages. For example, not only the generation of F radicals and/or XF_n , but also reaction between the generated F radicals and/or XF_n and the solid residues within the processing chamber, is substantially enhanced by provision of external energy to the processing chamber.
- [0090] In an alternative embodiment of the present invention, the precursor gases are mixed and reacted first in a separate mixing chamber immediately before entering the processing chamber. In this embodiment, the energy source supplies external energy to the mixing chamber.
- [0091] In order to control the reaction conditions and to achieve highly efficient cleaning action, temperature/pressure monitoring and controlling devices can be employed. Such devices are well known in the art, and one ordinarily skilled in the art will be able to determine suitable types of such devices without undue effort, according to specific operational conditions and requirements.
- [0092] The features and practice of the present invention are more fully appreciated with

respect to the following discussion.

[0093] Figure 1 shows an *in-situ* generation system 10, which comprises a fluorine source 1, a halogen source 2 for supplying halogen species such as Cl_2 , Br_2 , and/or I_2 , a delivery system 3, a mixing system 4, a semiconductor processing chamber 5, and energy sources 6. Fluorine gas and halogen species are provided by the fluorine source 1 and halogen source 2, respectively, and then transported to the mixing system 4 by the delivery system 3. Thermal or ultraviolet energy is supplied by energy source 6 to the mixing system for the purpose of enhancing reaction rate and production yield of XF_n compounds with higher F ratio. Reaction products comprising F radicals and/or XF_n compounds are then delivered into the semiconductor processing chamber 5 for removing solid residues inside such chamber. The fluorine gas and halogen species optionally and alternatively can be directly transported into the processing chamber 5 without passing the mixing system 4. In such case, the energy source 6 supplies thermal or ultraviolet energy to the processing chamber 5 in a direct manner.

[0094] Figure 2 shows another *in-situ* generation system 20, according to a preferred embodiment of the present invention. Fluorine gas and other halogen species are supplied by fluorine source 28 and halogen source 30, which are under operative control of flow control valves 22 and 24. When the flow control valves 22 and 24 are turned on, the fluorine gas and the halogen species are separately transported by fluid flow conduits 34 and 36, respectively, into mixing chamber 38. Precursor gases are mixed and reacted in the mixing chamber 38, under control of temperature control device 42 and pressure control device 44. UV source 40 applies UV-irradiation to mixing chamber 38 to facilitate reactions between the fluorine gas and the other halogen species.

[0095] Preferably, the UV source provides UV light at an intensity of from about 10^3 to about 10^6 W/m^2 .

[0096] Reaction products of fluorine gas and other halogen species are transported by fluid flow conduit 46 into a holding chamber 48. When internal pressure within the holding chamber 48 reaches a pre-determined level, mass flow controller 52 can be opened to allow flow of generated F radicals and/or XF_n compounds through fluid

flow conduit 50 into processing chamber 54 to clean interior of such processing chamber. After the cleaning process is completed, the effluent gas stream is discharged from the processing chamber 54 into an exhaust/abatement system 60 through fluid flow conduit 58.

[0097] The system also comprises a bypassing line 62 controlled by a bypassing valve 64 for flowing reaction products generated by the mixing chamber 38 directly into the exhaust/abatement system 60, without passing the processing chamber 54. Such bypassing line is useful for maintaining system stability during wafer-processing cycle when the processing chamber is isolated from the rest of the system (otherwise F radicals and/or XF_n compounds will contaminate the wafer products).

[0098] A diluent gas source 32 is also provided for supplying relatively inert gas, such as Ar, He, or N_2 , to dilute the F radicals and/or XF_n compounds delivered into the processing chamber 54. Such diluent gas source 32 is controlled by a flow control valve 26 as well as a mass flow controller 56. Diluent gas will effectively reduce reaction rates between the F radicals and/or XF_n compounds and the solid residues in the processing chamber 54, so as to avoid sudden pressure increase inside the processing chamber 54.

[0099] _____ Although the invention has been described herein with reference to specific features, aspects and embodiments, it will be appreciated that the applicability of the invention is not thus limited, but readily extends to and encompasses numerous variations, modifications and other embodiments, as will readily suggest themselves to those of ordinary skill in the art. Accordingly, the invention is to be broadly construed, consistent with the claims hereafter set forth.

[0100] OLE_LINK3